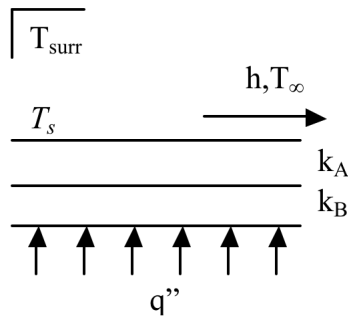
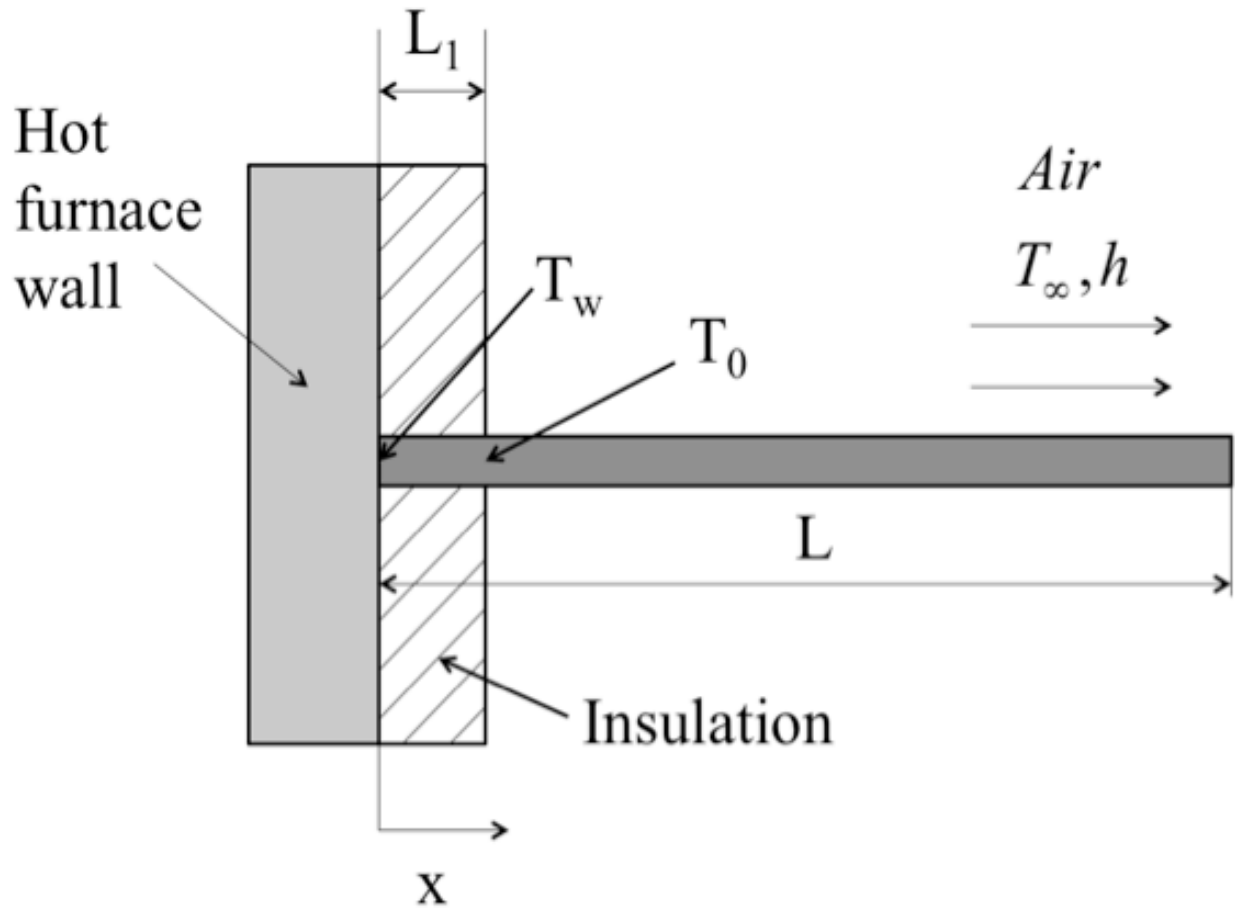


1. A heater is attached to the bottom of a compound plane (with regions A and B) with the top surface exposed to convection and radiation. The thermal conductivities of the two regions are  $k_A=10 \text{ W/m-K}$  and  $k_B=15 \text{ W/m-K}$ . The convective heat transfer coefficient is  $h=50 \text{ W/m}^2\text{-K}$ , and the fluid temperature is  $T_\infty=70 \text{ }^\circ\text{C}$ . The surrounding temperature is  $T_{surr}=27 \text{ }^\circ\text{C}$ . The temperature of top surface is  $T_s=66 \text{ }^\circ\text{C}$  and the thickness of each region is  $t=1 \text{ cm}$ . A constant heat flux  $q''$  is coming into the plane at the bottom surface. The plane can be considered a blackbody. Consider 1-D conduction in the compound plane.

- Draw an appropriate control volume for compound plane and write the energy balance equation.
- What is the value of constant heat flux  $q''$ ?
- Is radiation significant? Why (not)?
- Calculate the temperature at the interface of A and B and the bottom surface at steady state. Neglect any contact resistance.



2. A cylindrical rod of diameter  $D = 25 \text{ mm}$  and thermal conductivity of  $k = 100 \text{ W/m.K}$  protrudes normally from a furnace wall that is at  $T_w$ , and is covered by an insulation of thickness  $L_1 = 200 \text{ mm}$ . A uniform heat flux of  $45 \text{ kW/m}^2$  escapes through the furnace wall. This rod is welded to the furnace wall and is used as a hanger for supporting instrumentation cables. The exposed surface of the rod is cooled by natural convection by ambient air at  $25 \text{ }^\circ\text{C}$  with convection coefficient  $h = 20 \text{ W/m}^2\text{K}$ . The length of the rod is much larger than the diameter, so that the exposed portion of the rod can be considered to be an infinitely long fin.



- Sketch the temperature distribution within the rod from  $x=0$  to  $x=L$ .
- Compute the temperature of the furnace,  $T_w$  and the exposed surface temperature of the rod,  $T_0$ , at  $x=L_1$ .
- Compute the effectiveness and efficiency of the fin (the exposed portion of the rod).
- To avoid damaging the cables,  $T_0$  must be maintained below a specified operating limit of  $100^\circ\text{C}$ . Does this rod meet the operating conditions? How does  $T_0$  change with increase in (i) Rod diameter,  $D$ , (ii) Thermal conductivity of rod,  $k$ , and (iii) Thickness of the insulation,  $L_1$ ?

3. A sphere 30 mm in diameter initially at 800 K is quenched in a large bath having a constant temperature of 300 K with a convection heat transfer coefficient of 75 W/m<sup>2</sup>K. The thermal conductivity of the sphere material is  $k = 1.7$  W/mK and its thermal diffusivity of the sphere material is  $\alpha = 2.5 \times 10^{-6}$  m<sup>2</sup>/s.

(a) If we assume that the temperature of the sphere is uniform at any time (Lumped capacitance model *is valid*), calculate the time required for the sphere to reach 500 K.

For *parts (b) and (c)*, assume that the *lumped capacitance model is not valid*.

(b) Show, in a qualitative manner on T-t coordinates, the temperatures at the center and at the surface of the sphere as a function of time.

(c) Calculate the time required for the center of the sphere to reach 500 K.